



# The sum is more than its parts: stability of MnFe oxide nanoparticles supported on oxygen-functionalized multi-walled carbon nanotubes at alternating oxygen reduction reaction and oxygen evolution reaction conditions

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## Abstract

Successful design of reversible oxygen electrocatalysts does not only require to consider their activity towards the oxygen reduction (ORR) and the oxygen evolution reactions (OER), but also their electrochemical stability at alternating ORR and OER operating conditions, which is important for potential applications in reversible electrolyzers/fuel cells or metal/air batteries. We show that the combination of catalyst materials containing stable ORR active sites with those containing stable OER active sites may result in a stable ORR/OER catalyst if each of the active components can satisfy the current demand of their respective reaction. We compare the ORR/OER performances of oxides of Mn (stable ORR active sites), Fe (stable OER active sites), and bimetallic  $\text{Mn}_{0.5}\text{Fe}_{0.5}$  (reversible ORR/OER catalyst) supported on oxidized multi-walled carbon nanotubes. Despite the instability of Mn and Fe oxide for the OER and the ORR, respectively,  $\text{Mn}_{0.5}\text{Fe}_{0.5}$  exhibits high stability for both reactions.

**Keywords** Manganese oxide · Iron oxide · Multi-walled carbon nanotubes · Electrocatalysis · Stability · Bifunctional oxygen electrodes

Dedicated to Prof. Fritz Scholz on the occasion of his 65th birthday

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## Introduction

Development and commercialization of regenerative energy conversion technologies, such as rechargeable metal-air batteries or reversible electrolyzer-fuel cell devices, are presently challenged by a lack of electrochemically stable materials that are able to reversibly catalyze both the oxygen reduction (ORR) and the oxygen evolution (OER) reactions at low overpotentials. A typical strategy for the fabrication of bifunctional ORR/OER electrocatalytic materials consists in combining at least two types of active sites into a composite, one being highly active towards the ORR while the other exhibits high activity towards the OER, resulting in highly active bifunctional ORR/OER catalysts [1–5]. However, the widely demonstrated trade-off between activity and stability, that is, the fact that often highly active materials exhibit poor long-term stability and vice versa [6–8], is rarely taken in consideration during catalyst design. Although this is an issue that concerns electrocatalysis in general, bifunctional electrocatalysis faces an even more daunting challenge: it requires the use of not only highly active but also highly stable

catalytic materials able to operate in the long term at the conditions of not one but of two different reactions.

Investigation of electrochemical stability of bifunctional ORR/OER catalysts is often demonstrated in the literature at either ORR or OER conditions [9–13]. While this approach could indicate the suitability of the materials for either ORR or OER applications, it does not provide information about their applicability as reversible oxygen electrodes. Thus, a proper assessment of the stability of bifunctional ORR/OER catalysts aiming to reversible energy conversion applications requires the observation of time-dependent electrocatalytic behavior at alternating reaction conditions. This, however, results often in a fast and severe damage of ORR active sites during the reaction conditions of the OER, and/or vice versa, after a short time of exposure to the two reactions [14–19].

Taking into account the aforementioned considerations, we propose as a strategy for the design of reversible ORR/OER electrodes the combination of an active ORR catalyst inherently stable within the potential range of ORR operation, with an active OER catalyst inherently stable within the potential range of OER operation. If the active sites of the former are able to satisfy the current demand of the electrochemical system during the ORR, it will kinetically govern the catalytic process without the aid of the latter, resulting in the protection of its active sites, and vice versa (Scheme 1).

## Experimental

### Catalyst synthesis and characterization

Synthesis of  $\text{MO}_x/\text{MWCNTs-Ox}$ -type catalysts has been reported previously [20]. In brief, growing of multi-walled carbon nanotubes (MWCNTs) was conducted by chemical vapor deposition of ethylene at a temperature of 680 °C using an Fe-Co growth catalyst [21, 22]. The majority of catalyst residues were removed by treating the MWCNTs in a boiling aqueous HCl solution (15 vol%) for 4 h under strong stirring [23], after which the MWCNTs were washed with distilled water until neutral pH. The dried MWCNTs were then treated in concentrated  $\text{HNO}_3$  for 2 h while constantly stirring the mixture to

introduce oxygen functionalities [24]. Subsequently, the oxygen-functionalized MWCNTs (MWCNTs-Ox) were washed with distilled water until neutral pH. After drying in air, MWCNTs-Ox were modified with Mn and Fe via incipient wet impregnation for 12 h using aqueous solutions of either  $\text{Fe}(\text{NO}_3)_3$ ,  $\text{Mn}(\text{NO}_3)_2$  as precursors, or a mixture of them at a 1:1 molar ratio. The impregnated materials were dried at 110 °C for 4 h and subsequently annealed under argon flow at 350 °C for 4 h to form the metal oxide nanoparticles. The overall metal loading of the catalysts was about 14 wt%.

Structural characterization has been reported previously [3, 20] and is summarized in Table S1.

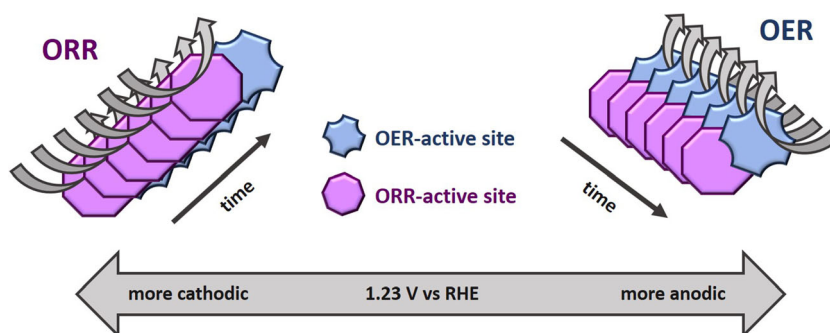
Complementary Raman spectroscopy measurements were conducted with a Jubin-Yvon iHR550 spectrometer (HORIBA) equipped with a laser source of  $\lambda = 532$  nm (Ventus 532, Laser Quantum) and a laser power of 2 mW.

$\text{N}_2$  adsorption isotherms, used for the determination of specific surface area, were obtained at a temperature of 77 K using an ASAP-2400 instrument (Micromeritics).

### Electrochemical characterization

Electrochemical experiments were conducted in a three-electrode configuration rotating disk electrode setup using an Autolab PGSTAT128N potentiostat/galvanostat (Metrohm) equipped with an RDE 80793 rotator (Metrohm). Catalyst inks were prepared by dispersing 5  $\text{mg mL}^{-1}$  active material in a mixture of water, ethanol, and Nafion (49:49:2 volume ratio) for 15 min via sonication. Glassy carbon rotating disk electrodes (RDEs) of 0.113  $\text{cm}^2$  geometric area were polished using 0.05  $\mu\text{m}$   $\text{Al}_2\text{O}_3$  paste, and subsequently cleaned by placing them in a mixture of ethanol and water (1:1 volume ratio) followed by ultrasonication for 1 min. The RDEs were modified by drop-casting 4.8  $\mu\text{L}$  catalyst ink to achieve a total catalyst loading of 210  $\mu\text{g cm}^{-2}$ . After drying at room temperature under static air, the modified RDEs were used as the working electrode. A platinum mesh maintained during the measurements in a compartment separated by a glass frit was used as counter electrode. The reference electrode was a double-junction Ag/AgCl/KCl (3 M) electrode (Metrohm). An aqueous 0.1 M KOH solution saturated with oxygen was

**Scheme 1** Representation of the protection effect of active sites over time in reversible ORR/OER catalysts



used as the electrolyte. Prior to measurements, metal impurities contained in the electrolyte were removed by means of a Chelex cation-exchange resin (Bio-Rad Laboratories) [25]. After setup and before all measurements, the electrodes were subjected to continuous potential cycling between  $-0.6$  and  $0.5$  V vs. Ag/AgCl/KCl (3 M) at a scan rate of  $100 \text{ mV s}^{-1}$  until a constant response was observed. Subsequently, an electrochemical impedance spectrum (EIS) was recorded at open circuit potential in the frequency range between  $100 \text{ kHz}$  and  $10 \text{ Hz}$  with an AC amplitude of  $10 \text{ mV}$  (RMS) for the determination of the uncompensated resistance.

The electrocatalytic activity of the investigated catalysts towards the ORR and the OER was evaluated by means of RDE voltammetry by recording linear sweep voltammograms in the potential range from  $0.1$  to  $-0.9$  V vs. Ag/AgCl/KCl (3 M), and from  $0.0$  to  $0.8$  V vs. Ag/AgCl/KCl (3 M), respectively, with a scan rate of  $5 \text{ mV s}^{-1}$  and an electrode rotation of  $1600 \text{ rpm}$ . Activity measurements were done in triplicate and the average of the three measurements was reported.

Stability tests were conducted chronopotentiometrically in an RDE setup for  $60 \text{ min}$  by alternately applying two current densities, switching from one to the other each  $2 \text{ min}$ , while maintaining an electrode rotation of  $1600 \text{ rpm}$ . The current densities applied were  $0$  and  $-1 \text{ mA cm}^{-2}$ ,  $0$  and  $+10 \text{ mA cm}^{-2}$ , or  $-1$  and  $+10 \text{ mA cm}^{-2}$ , to assess the stability during ORR, OER, and reversible ORR/OER, respectively. The applied currents were held for  $5 \text{ s}$  before start recording the electrode potentials.

Taking the pH of the electrolyte, the current measured ( $i$ ), and the uncompensated resistance ( $R_u$ ) into consideration, all measured potentials were  $iR_u$ -drop corrected and converted to the RHE scale according to Eq. 1.

$$E_{\text{RHE}} = E_{\text{Ag/AgCl/KCl}} + 0.207 + 0.059 \cdot \text{pH} - iR_u \quad (1)$$

The pH of the electrolyte was determined with a CP-411 pH-meter (Elmetron).  $R_u$  was extracted from the Nyquist plots obtained from EIS measurement for each electrode film.

## Results and discussion

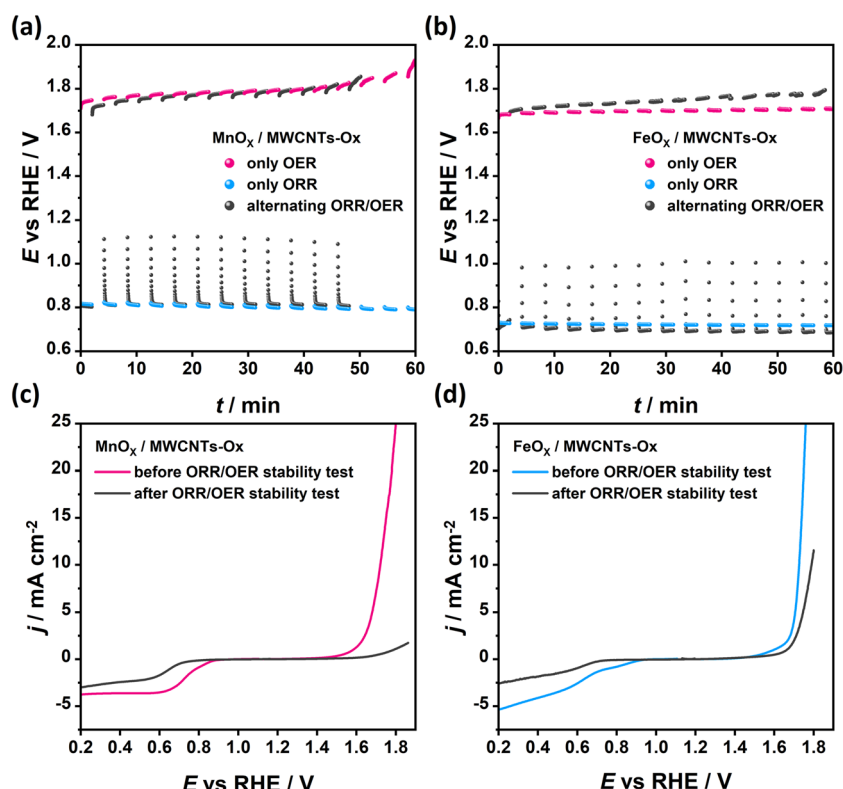
To demonstrate the proposed hypothesis, the electrochemical stability of oxides of Mn and Fe supported on oxygen-functionalized multi-walled carbon nanotubes, hereafter denoted as  $\text{MnO}_x/\text{MWCNTs-Ox}$  and  $\text{FeO}_x/\text{MWCNTs-Ox}$ , respectively, was investigated. Synthesis and characterization of the two catalysts have been previously reported [3, 20] and are summarized in Table S1. The catalysts were subjected to three different chronopotentiometric protocols to evaluate their stability at either (i) only OER, (ii) only ORR, or (iii) alternating ORR/OER conditions by applying alternately two current densities, each for  $2 \text{ min}$ , maintaining the alternation for a total

of  $1 \text{ h}$ . The current densities applied were (i)  $+10$  and  $0 \text{ mA cm}^{-2}$  (only OER); (ii)  $-1$  and  $0 \text{ mA cm}^{-2}$  (only ORR); and (iii)  $-1$  and  $+10 \text{ mA cm}^{-2}$  (alternating ORR/OER). All stability tests were conducted in triplicate. The individual measurements (Fig. S1) and a short discussion concerning reproducibility have been included in the Supporting Information. Figure 1 a and b show the electrode potentials recorded for  $\text{MnO}_x/\text{MWCNTs-Ox}$  and  $\text{FeO}_x/\text{MWCNTs-Ox}$ , respectively, as a function of time, and are displayed with the same scale to facilitate comparison between ORR and OER overpotentials exhibited by the two catalysts. As shown in Fig. 1a,  $\text{MnO}_x/\text{MWCNTs-Ox}$  displayed a substantial deactivation during the only OER stability test, with an increase of overpotential of about  $160 \text{ mV}$  after  $1 \text{ h}$ . In contrast, the same catalyst exhibited a stable behavior during only ORR, with no substantial change of the measured potential throughout the measurement. The response observed during the stability test in which ORR and OER were conducted alternately did not differ considerably from those in which ORR and OER were done independently. In contradistinction,  $\text{FeO}_x/\text{MWCNTs-Ox}$  exhibited a more stable response than  $\text{MnO}_x/\text{MWCNTs-Ox}$  during the only OER stability measurement, with an increase of overpotential of less than  $20 \text{ mV}$  after  $1 \text{ h}$ , whereas an increase of ORR overpotential of less than  $20 \text{ mV}$  was observed by the end of the only ORR stability test (Fig. 1b). However, the response observed for  $\text{FeO}_x/\text{MWCNTs-Ox}$  when alternating between the ORR and OER displayed a considerably larger deactivation for both the OER and ORR, with increasing overpotentials of about  $90$  and  $40 \text{ mV}$ , respectively, after  $1 \text{ h}$ .

Linear sweep voltammograms of  $\text{MnO}_x/\text{MWCNTs-Ox}$  and  $\text{FeO}_x/\text{MWCNTs-Ox}$  were recorded before and after ORR/OER stability test and are shown in Fig. 1 c and d, respectively. The potentials recorded at current density values of  $-1 \text{ mA cm}^{-2}$  ( $E_{\text{ORR}}$ ) and  $+10 \text{ mA cm}^{-2}$  ( $E_{\text{OER}}$ ), as well as the difference between these two ( $\Delta E = E_{\text{OER}} - E_{\text{ORR}}$ ), were found to be in agreement with those observed during the first ORR/OER alternation in the stability measurements (Table S2). To facilitate the comparison of the activity of these materials with other ORR and bifunctional ORR/OER catalysts reported in the literature, the potentials at which a current density of  $-3 \text{ mA cm}^{-2}$  was achieved and the resulting  $\Delta E$  values are shown in Table S3. Voltammograms recorded at the end of the stability test displayed a clear increase in overpotential towards both the OER and the ORR. Discrepancies between  $E_{\text{ORR}}$  and  $E_{\text{OER}}$  values from the voltammograms and those from the last cycle of their corresponding chronopotentiometric measurements may be due to, e.g., an increase of damage of active sites, partial catalyst detachment, and accumulation of oxygen gas bubbles on the electrode surface [26].

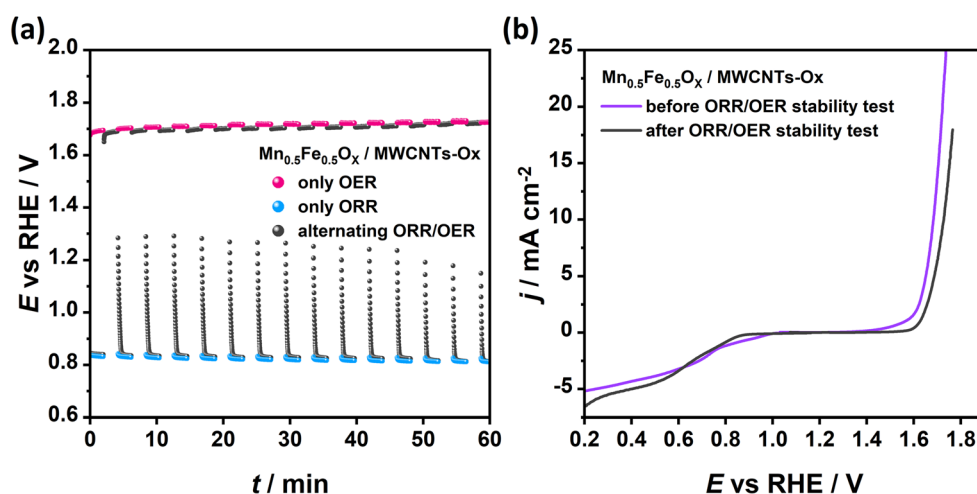
The stability measurements showed that both  $\text{MnO}_x/\text{MWCNTs-Ox}$  and  $\text{FeO}_x/\text{MWCNTs-Ox}$  perform poorly as reversible ORR/OER catalysts. Nevertheless,  $\text{MnO}_x/\text{MWCNTs-Ox}$

**Fig. 1** Stability of **a**  $\text{MnO}_x/\text{MWCNTs-Ox}$  and **b**  $\text{FeO}_x/\text{MWCNTs-Ox}$  measured chronopotentiometrically by alternating each 2 min either between  $-1$  and  $0 \text{ mA cm}^{-2}$  (only ORR), between  $10$  and  $0 \text{ mA cm}^{-2}$  (only OER), or between  $-1$  and  $10 \text{ mA cm}^{-2}$  (alternating ORR/OER), for a total duration of  $1 \text{ h}$ . Data recorded at  $0 \text{ mA cm}^{-2}$  is not shown. Linear sweep voltammograms of **c**  $\text{MnO}_x/\text{MWCNTs-Ox}$  and **d**  $\text{FeO}_x/\text{MWCNTs-Ox}$  recorded at  $5 \text{ mV s}^{-1}$  scan rate before and after the alternating stability test. All measurements were conducted in  $\text{O}_2$ -saturated  $0.1 \text{ M KOH}$  with an electrode rotation of  $1600 \text{ rpm}$



$\text{MnO}_x/\text{MWCNTs-Ox}$  showed comparatively higher stability during the ORR than  $\text{FeO}_x/\text{MWCNTs-Ox}$ , and vice versa,  $\text{FeO}_x/\text{MWCNTs-Ox}$  displayed a more stable response than  $\text{MnO}_x/\text{MWCNTs-Ox}$  during the OER. According to the proposed hypothesis, a combination of the two catalysts, one being stable for ORR and the other being stable for OER, would result in a bifunctional catalyst of superior stability at alternating ORR/OER conditions as compared with that of its monometallic components. Consequently, we used the bimetallic

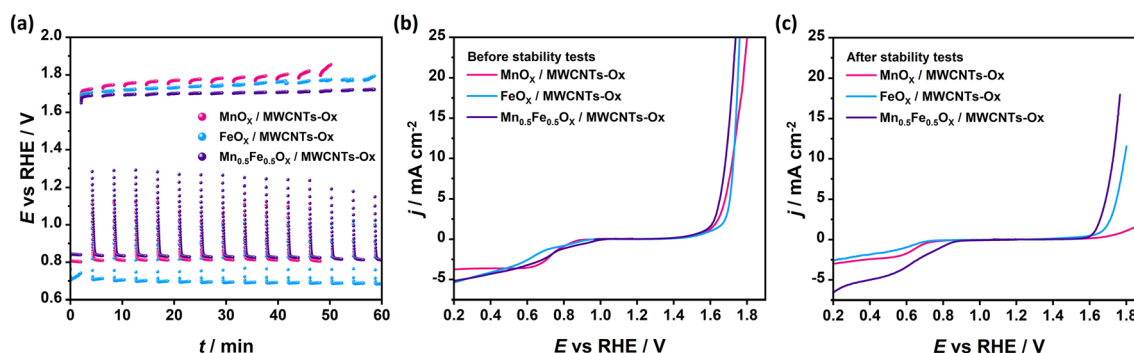
catalyst  $\text{Mn}_{0.5}\text{Fe}_{0.5}\text{O}_x/\text{MWCNTs-Ox}$  in the same chronopotentiometric stability tests. As shown in Fig. 2a, increases in OER and ORR overpotentials of about  $30$  and  $25 \text{ mV}$ , respectively, were observed after  $1 \text{ h}$ , regardless of whether the ORR and OER were conducted separately or alternately. Linear sweep voltammograms recorded before and after ORR/OER stability measurements are shown in Fig. 2b demonstrating the superior stability of  $\text{Mn}_{0.5}\text{Fe}_{0.5}\text{O}_x/\text{MWCNTs-Ox}$



**Fig. 2** **a** Stability of  $\text{Mn}_{0.5}\text{Fe}_{0.5}\text{O}_x/\text{MWCNTs-Ox}$  measured chronopotentiometrically by alternating each  $2 \text{ min}$  either between  $-1$  and  $0 \text{ mA cm}^{-2}$  (only ORR), between  $10$  and  $0 \text{ mA cm}^{-2}$  (only OER), or between  $-1$  and  $10 \text{ mA cm}^{-2}$  (alternating ORR/OER) for a total of  $1 \text{ h}$ .

Data recorded at  $0 \text{ mA cm}^{-2}$  is not shown. **b** Linear sweep voltammograms recorded at  $5 \text{ mV s}^{-1}$  scan rate before and after stability test. All measurements were conducted in  $\text{O}_2$ -saturated  $0.1 \text{ M KOH}$  solution with an electrode rotation of  $1600 \text{ rpm}$





**Fig. 3** Comparison of stability and activity of  $\text{MO}_x/\text{MWCNTs-Ox}$ , with  $\text{M} = \text{Mn}$ ,  $\text{Fe}$ , and  $\text{Mn}_{0.5}\text{Fe}_{0.5}$ . **a** Electrochemical stability measured chronopotentiometrically by alternating each 2 min between  $-1$  and  $+10 \text{ mA cm}^{-2}$  for a total of 1 h. Linear sweep voltammograms recorded at a

scan rate of  $5 \text{ mV s}^{-1}$  **b** before and **c** after stability tests. All measurements were conducted in  $\text{O}_2$ -saturated  $0.1 \text{ M KOH}$  solution with an electrode rotation of  $1600 \text{ rpm}$

$\text{MWCNTs-Ox}$  as compared with that of  $\text{MnO}_x/\text{MWCNTs-Ox}$  and  $\text{FeO}_x/\text{MWCNTs-Ox}$  (Fig. 1 c and d, respectively).

A comparison between the ORR/OER performances in terms of stability and activity exhibited by the three investigated catalysts is shown in Fig. 3. The bimetallic catalyst  $\text{Mn}_{0.5}\text{Fe}_{0.5}\text{O}_x/\text{MWCNTs-Ox}$  exhibited not only a substantial higher stability, but also lower overpotentials for both the ORR and OER compared with the monometallic materials, both at the beginning and at the end of the stability measurements. The activity enhancement has been previously discussed [3] and is ascribable to the formation of more active catalytic sites, for instance  $\text{MnFe}_2\text{O}_4$  (Table S1), as well as synergistic interactions upon combining the different metal components. The presence of more active catalytic sites seemed to facilitate the supply of current over time during the OER, whereas in the case of the ORR, the observed response did not differ substantially from that of  $\text{MnO}_x/\text{MWCNTs-Ox}$  as the measurement progressed. This observation indicates that  $\text{MnO}_x$  remained the main catalytic site for the ORR and was indeed able to satisfy the current demand for this reaction entirely, thus protecting the OER active sites from reductive damage. In the same way, due to the kinetic advantage of the OER catalytic sites, the ORR active sites were protected during the OER as long as the OER sites were able to provide the required current.

## Conclusions

We propose a strategy for the design of reversible ORR/OER electrocatalyst by combining inherently stable ORR active sites with inherently stable OER active sites, each of them being capable to supply the current demand of the electrochemical system without the aid of the other. The strategy was demonstrated with the investigation of the electrochemical stability of  $\text{Mn}$ ,  $\text{Fe}$ , and  $\text{Mn}_{0.5}\text{Fe}_{0.5}$  oxides supported on oxidized multi-walled carbon nanotubes at alternating ORR/OER conditions.  $\text{Mn}$  oxide exhibited high stability during

ORR, but its activity decreased fast when exposed to the highly anodic OER potentials.  $\text{Fe}$  oxide displayed a comparatively higher stability towards the OER than  $\text{Mn}$  oxide; however, a substantial increase of both ORR and OER overpotentials was observed at alternating ORR/OER. In agreement with our hypothesis,  $\text{Mn}_{0.5}\text{Fe}_{0.5}$  oxide exhibited a superior electrochemical stability than the monometallic catalysts at alternating ORR/OER. Although these results suggest that the stability enhancement is due to the kinetic advantage of OER active sites over ORR active sites during OER, or vice versa during ORR, structural characterization of the investigated catalysts at *operando* conditions is still required to fully reveal the nature of the observed stability enhancement.

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**Code availability** Not applicable (software application or custom code).

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**Data availability** All data are stored on a server with frequent backup.

## Compliance with ethical standards

**Conflict of interest** The authors declare that they have no conflict of interest.

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